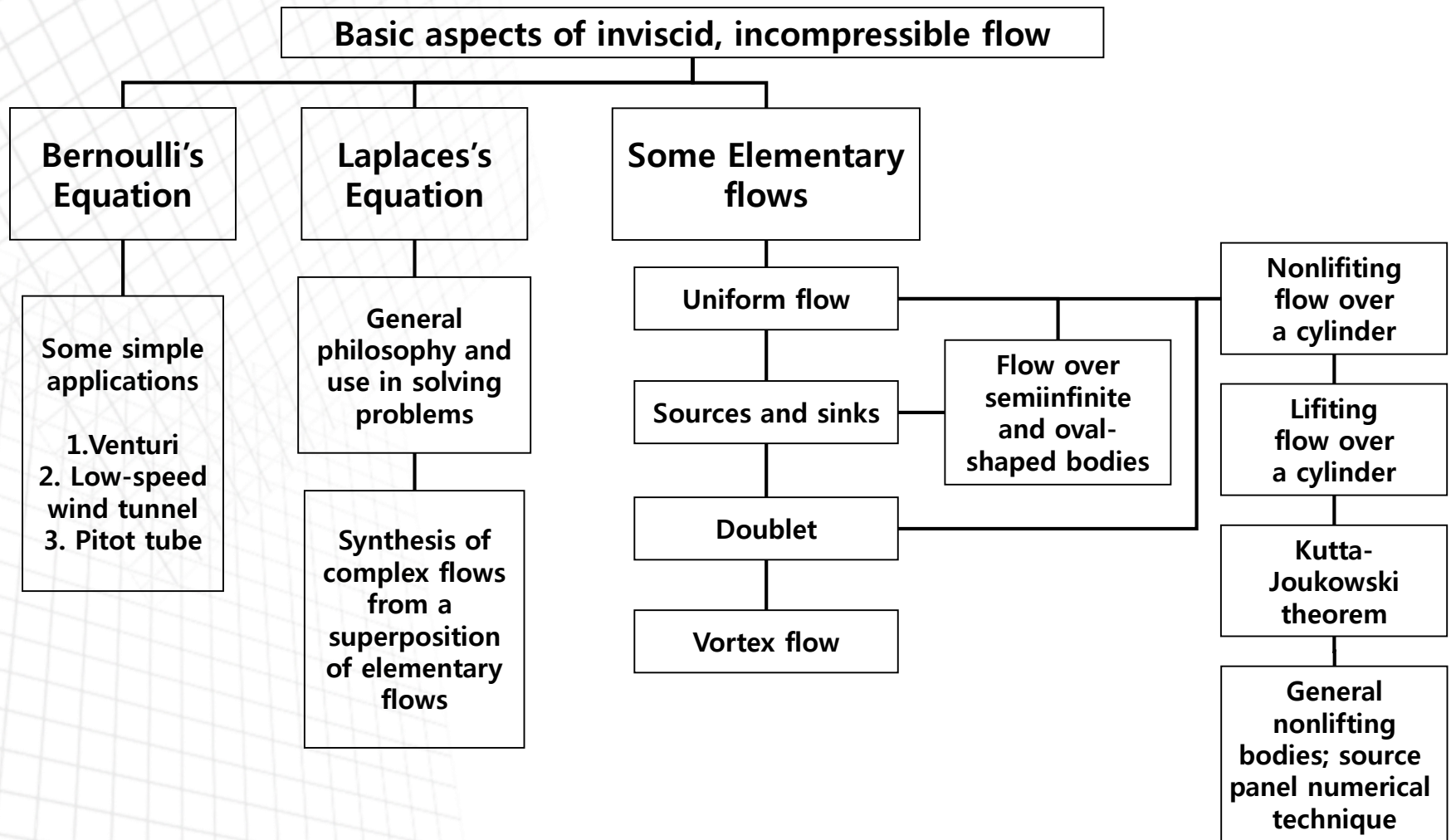


# *Inviscid & Incompressible flow*

## < 3.1. Introduction and Road Map >



# Inviscid & Incompressible flow

## < 3.2. Bernoulli's Equation >

### ❖ From the momentum equation

$$\rho \frac{\partial \vec{V}}{\partial t} + (\vec{V} \cdot \nabla) \rho \vec{V} = -\nabla p + \rho \vec{f} + F_{viscous}$$

### ❖ For an inviscid and steady flow without no body force

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial x} \quad : \text{x-dir. Momentum equation}$$

## < 3.2. Bernoulli's Equation >

### ❖ Multiply dx

$$u \frac{\partial u}{\partial x} dx + v \frac{\partial u}{\partial y} dx + w \frac{\partial u}{\partial z} dx = - \frac{1}{\rho} \frac{\partial p}{\partial x} dx$$

### ❖ From the equation of streamline

$$udz - wdx = 0$$

$$vdx - udy = 0$$

$$\rightarrow u \left( \frac{\partial u}{\partial x} dx + \frac{\partial u}{\partial y} dy + \frac{\partial u}{\partial z} dz \right) = - \frac{1}{\rho} \frac{\partial p}{\partial x} dx$$

## < 3.2. Bernoulli's Equation >

$$u\left(\frac{\partial u}{\partial x}dx + \frac{\partial u}{\partial y}dy + \frac{\partial u}{\partial z}dz\right) = -\frac{1}{\rho}\frac{\partial p}{\partial x}dx$$

$$\rightarrow udu = -\frac{1}{\rho}\frac{\partial p}{\partial x}dx$$

$$\rightarrow \frac{1}{2}d(u^2) = -\frac{1}{\rho}\frac{\partial p}{\partial x}dx \quad : \text{x-dir.}$$

Similarly,  $\frac{1}{2}d(v^2) = -\frac{1}{\rho}\frac{\partial p}{\partial y}dy \quad : \text{y-dir.}$

$$\frac{1}{2}d(w^2) = -\frac{1}{\rho}\frac{\partial p}{\partial z}dz \quad : \text{z-dir.}$$

## < 3.2. Bernoulli's Equation >

$$\rightarrow \frac{1}{2}d(u^2 + v^2 + w^2) = -\frac{1}{\rho}dp$$

$$\rightarrow dp = -\rho VdV \quad \text{along a streamline}$$

If incompressible,  $\int_1^2 dp = -\rho \int_1^2 VdV \rightarrow p_2 - p_1 = -\rho\left(\frac{V_2^2}{2} - \frac{V_1^2}{2}\right)$

$$\therefore p_1 + \frac{1}{2}\rho V_1^2 = p_2 + \frac{1}{2}\rho V_2^2 \rightarrow p + \frac{1}{2}\rho V^2 = \text{const} \quad \text{along a streamline}$$

If irrotational,  $p + \frac{1}{2}\rho V^2 = \text{const}$  everywhere

## < 3.3. The Venturi and Low-Speed Wind Tunnel >

### ❖ Venturi tube

#### ● Assume)

- 1. Quasi-one-dimensional flow  
(the properties are uniform across the x-section)
- 2. Inviscid flow
- 3. Steady flow

#### ● Continuity equation

$$\frac{\partial}{\partial t} \iiint_V \rho dV + \iint_S \rho \vec{V} \cdot d\vec{S} = 0$$

steady  $\swarrow$

$$\rightarrow \iint_{A_1 + A_2 + wall} \rho \vec{V} \cdot d\vec{S} = 0$$

## < 3.3. The Venturi and Low-Speed Wind Tunnel >

### ❖ Venturi tube

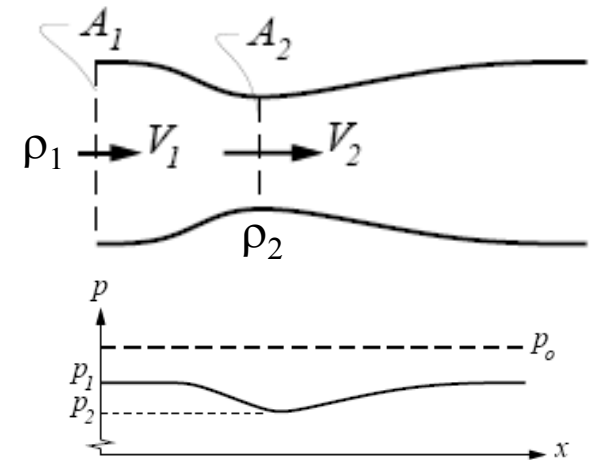
$$\iint_{A_1 + A_2 + wall} \rho \vec{V} \cdot d\vec{S} = 0$$

$$\iint \rho \vec{V} \cdot d\vec{S} = 0 \text{ at the wall}$$

$$1 : \iint_{A_1} \rho \vec{V} \cdot d\vec{S} = -\rho_1 A_1 V_1$$

$$2 : \iint_{A_2} \rho \vec{V} \cdot d\vec{S} = \rho_2 A_2 V_2$$

$$\therefore \rho_1 A_1 V_1 = \rho_2 A_2 V_2$$



## < 3.3. The Venturi and Low-Speed Wind Tunnel >

### ❖ Venturi tube

Incompressible  $\rightarrow A_1 V_1 = A_2 V_2$

Use two equations

1. Continuity eq.  $AV = \text{const}$

2. Bernoulli's eq.  $p + \frac{1}{2}\rho V^2 = \text{const}$

$$\rightarrow V_1^2 = \frac{2}{\rho}(p_2 - p_1) + V_2^2 = \frac{2}{\rho}(p_2 - p_1) + \left(\frac{A_1}{A_2} V_1\right)^2$$

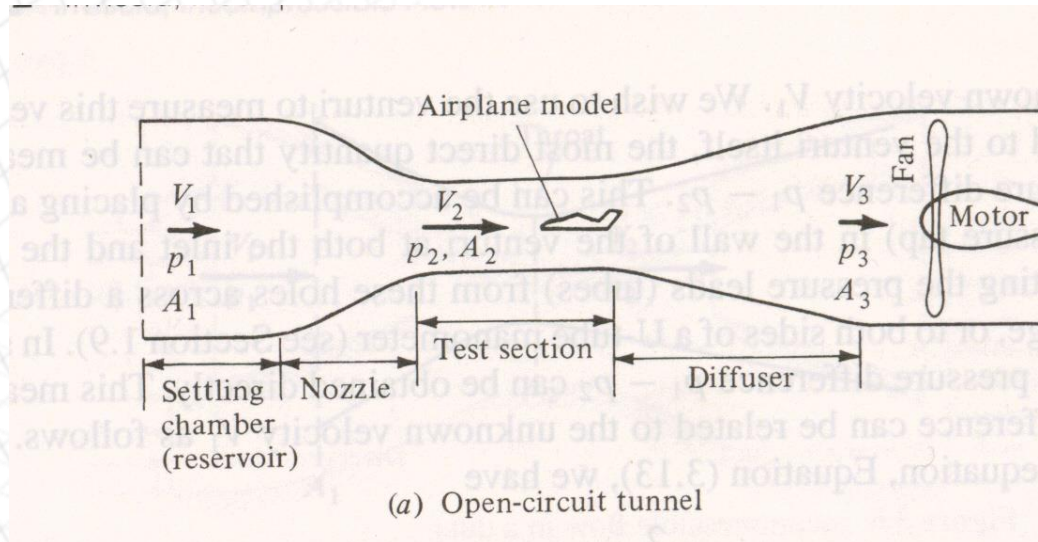
$$\therefore V_1 = \sqrt{\frac{2(p_2 - p_1)}{\rho\left[\left(\frac{A_1}{A_2}\right)^2 - 1\right]}}$$



# Inviscid & Incompressible flow

## < 3.3. The Venturi and Low-Speed Wind Tunnel >

### ❖ Low-speed wind tunnel



$$V_2 = \sqrt{\frac{2(p_1 - p_2)}{\rho[1 - (A_2/A_1)^2]}}$$

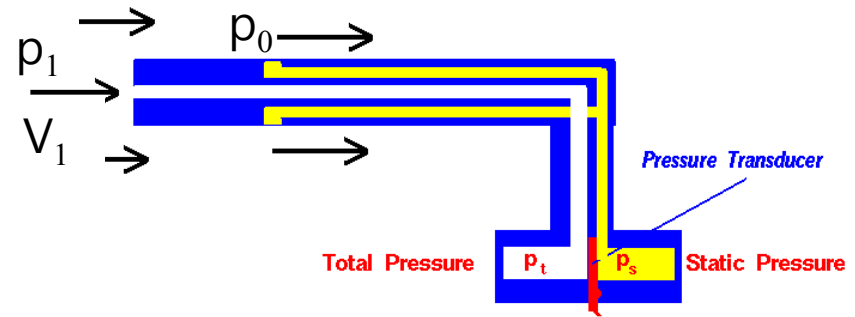
How to measure the pressure difference?

→ Manometer

# Inviscid & Incompressible flow

## < 3.4. Pitot Tube >

### ❖ Low-speed wind tunnel



$$V_1 = \sqrt{\frac{2(p_0 - p_1)}{\rho}}$$

$$\text{Dynamic pressure} \rightarrow \frac{1}{2} \rho V_1^2 + \text{Static pressure} \rightarrow p_1 = p_0 \leftarrow \text{Total pressure}$$

## < 3.5. Pressure Coefficient >

### ❖ Low-speed wind tunnel

$$C_p \equiv \frac{p - p_\infty}{\frac{1}{2} \rho V_\infty^2} \quad : \text{Over all the range of speed}$$

For incompressible flow

$$p_\infty + \frac{1}{2} \rho V_\infty^2 = p + \frac{1}{2} \rho V^2 \quad \rightarrow \quad p - p_\infty = \frac{1}{2} \rho (V_\infty^2 - V^2)$$

$$C_p = \frac{p - p_\infty}{q_\infty} = \frac{\frac{1}{2} \rho (V_\infty^2 - V^2)}{\frac{1}{2} \rho V_\infty^2} = 1 - \left(\frac{V}{V_\infty}\right)^2$$

$$\therefore C_p = 1 - \left(\frac{V}{V_\infty}\right)^2 \quad : \text{works for } M < 0.3 \text{ (low subsonic)}$$

$$* \text{ freestream } \rightarrow C_p = 0 \quad * \text{ stagnation point } \rightarrow C_p = 1$$

## < 3.6. Condition on Velocity for Incompressible Flow

>

### ❖ Continuity equation

Incompressible  $\rightarrow$   $\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{V}) = 0$

$$\rightarrow \therefore \nabla \cdot \vec{V} = 0$$

## < 3.7. Laplace's Equation >

$$\begin{aligned} \nabla \cdot \vec{V} &= 0 \\ \vec{V} &= \nabla \phi \end{aligned} \quad \rightarrow \quad \nabla \cdot (\nabla \phi) = \nabla^2 \phi = 0 \quad \rightarrow \text{Laplace's equation}$$

\* In 2D,

$$\nabla^2 \phi = \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} = 0$$

\* In irrotational flow,

$$\begin{aligned} \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} &= 0 \\ \frac{\partial}{\partial x} \left( -\frac{\partial \psi}{\partial x} \right) - \frac{\partial}{\partial y} \left( \frac{\partial \psi}{\partial y} \right) &= 0 \\ \frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} &= 0 \end{aligned}$$

Note)

1. For irrotational, incompressible flow, and are both solutions of Laplace equation.
2. Since Laplace equation is linear, the solution can be superimposed, so that any complex flow is expressed by adding elementary.

## < 3.7. Laplace's Equation >

i) Infinity B.C.

$$u = \frac{\partial \psi}{\partial x} = \frac{\partial \psi}{\partial y} = V_\infty$$

$$v = \frac{\partial \psi}{\partial y} = -\frac{\partial \psi}{\partial x} = 0$$

ii) wall B.C.

$$\left(\frac{v}{u}\right)_{wall} = \left(\frac{dy_b}{dx}\right) \leftarrow \text{Flow tangency condition}$$

slope of the streamline

